

IN THE CLAIMS

The following is a listing of all claims in the application with claims 4 and 5 shown as amended.

LISTING OF CLAIMS

1. (Withdrawn) A production process for methanol comprising a synthetic gas production step in which hydrocarbon is reacted with steam to generate synthetic gas comprising main components of hydrogen, carbon monoxide and carbon dioxide, a methanol synthesis step in which said synthetic gas is reacted on a methanol synthesis catalyst and resulting crude methanol is recovered in the form of liquid, and a distillation step in which said recovered crude methanol is distilled to be separated into waste water containing low boiling organic compounds and high boiling organic compounds and refined methanol, wherein used in said methanol synthesis step is a reactor which comprises a reaction tube, an inner tube closed at a lower end thereof disposed almost in the center of the reaction tube, a central tube in which unreacted feed gas flows disposed almost in the center of the inner tube, and a circular catalyst layer charged with a granular catalyst disposed in a circular space surrounded by the reaction tube and the inner tube and in which said central tube is disposed almost in the center of a wholly or partially detachable shielding plate provided at the upper end of the reaction tube.

2. (Withdrawn) The production process for methanol as described in claim 1, wherein in the methanol step, the synthetic gas is reacted on the methanol syntheses catalyst at a reaction pressure of 80 to 120 kg/cm².G, and crude methanol is recovered in the form of liquid.

3. (Withdrawn) The production process for methanol as described in claim 1, wherein in the methanol synthesis step, the synthetic gas is reacted on the methanol synthesis catalyst at a catalyst layer inlet temperature of 180 to 260° C, and crude methanol is recovered in the form of liquid.

4. (Currently Amended) A reactor for methanol synthesis comprising a reactor casing having an inlet end and an outlet end with the reactor casing having at least one or more reaction tubes of substantially equal length with upper and lower ends tube disposed on the inside thereof in a coaxial symmetrical arrangement symmetrically spaced apart from the reactor casing and being in communication with an upper chamber into which

unreacted gas is fed into said casing through said inlet end; each reaction tube having an inner tube disposed almost in the center of the reaction tube to form a first passageway of circular cross section between the inner tube and the surrounding reaction tube with the inner tube being closed at a lower end thereof facing a lower chamber located at a location symmetrically opposite said upper chamber and being open at the upper end to said first passageway, said reactor having a single charge of granular catalyst with said charge being stored in said first passageway to form a catalyst charged part therein surrounded by said one or more reaction tubes reaction tube; a central tube disposed almost in the center of the reactor inner tube with the central tube extending downwardly from said upper chamber a fixed distance above the said lower end of said reaction tube for forming a second passageway of circular cross section between said central tube and an said inner tube; an upper shielding plate for partitioning the upper end of said reaction tubes tube from said upper chamber, tube plates separating the reaction tubes tube from said reactor casing with said upper and lower chambers each defining a confined space of predetermined volume at symmetrically opposite ends of said reactor to facilitate a smooth flow of gas therethrough, wherein said unreacted gas flows downwards from said upper chamber through the upper part of the central tube flowing from said second passageway through said catalyst in said first passageway from the upper end of said first passageway and discharges from an outlet located in said lower end and wherein the length of said central tube is between 1/10 to 2/3 of the length of a the reaction tube measured from the upper end of the reaction tube.

5. (currently amended) The reactor for methanol synthesis as described in claim 4, wherein the inner tube is disposed almost vertically in said reactor reaction tube.

6. (Cancelled)